Mansoura Engineering Journal

Volume 19 | Issue 2

Article 2

6-1-2021

Stability and Control for Interconnected Multivariable Systems.

El-Sayed El-Konayaly Control & Computers Engineering Department., Faculty of Engineering., El-Mansoura University., Mansoura., Egypt.

Kamel Soliman Process Control & Inst. Dept Ammonia Plant., Semadco., Talkha.

Follow this and additional works at: https://mej.researchcommons.org/home

Recommended Citation

El-Konayaly, El-Sayed and Soliman, Kamel (2021) "Stability and Control for Interconnected Multivariable Systems.," *Mansoura Engineering Journal*: Vol. 19 : Iss. 2 , Article 2. Available at: https://doi.org/10.21608/bfemu.2021.163413

This Original Study is brought to you for free and open access by Mansoura Engineering Journal. It has been accepted for inclusion in Mansoura Engineering Journal by an authorized editor of Mansoura Engineering Journal. For more information, please contact mej@mans.edu.eg.

STABILITY AND CONTROL

FOR INTERCONNECTED MULTIVARIABLE SYSTEMS دراسة الإتزان والتحكم في الأنظمة المركبة

متعددة المتغير ات

By

E. H. E1-KONAYALY, K. M. SOLIMAN

Control & Computers Dept. , Faculty of Eng., El-Mansoura Univ. N. MEEKAWY process control & In st. Dept., Ammonia plant, Semadco, Talkha

يقلم البحث دراسة وتحليل وتصديم نظام تحكم لعملية كيميائية صناعية تمثل وحدة من وحدات عملية تخليق الأمونيا بمصنع سماد اليوريا بطلخا ، حيث يعتبر هذا النظام مركبا ومتعدد المتغيرات بالإضافة إلى وجود عوامل ربط داخلية بين مكوناتد . وحيث أن النموذج الرياضي للنظام عبارة عن علاقة زمنية مباشرة بين المدخلات والمخرجات ، فقد تم تحويل هذه الصيعة إلى صيغة ال ARMA MODEL التي تتناسب مع التحليل والتصميم باستخدام الحاسبات الرقمية . كما يقدم البحث دراسة دقيقة حول عوامل الربط بين مفردات النموذج وتأثيرها على الإتزان الكلي للنظام في حالة دائرة التحكم المفتوحة وبالتالي تصميم وحدات إضافية ثابتة تضاف إلى عوامل الربط لضمان عدم تأثيرها على الإتزان الكلي للنظام المركب وتأثيرا الحلي النظام الربط لضمان عدم تأثيرها على الإتزان الكلي للنظام الركب

وتتم هذه العملية باستخدام الطريقة المعروفة باسم "مصفوفة الكسب النسبي". كما تم تصميم عملية المحكم بدائرة مغلقة وتغذية خلفية بإستخدام طريقة "تخصيص الأقطاب" ، والتي أدت إلى نتائج جيدة تعزز فعالية النظام المقترح.

ABSTRACT.

The paper presents the analysis and control for an interconnected multivariable system, which simulates the behaviour of a subsystem of real chemical ammonia conversion process in SEMADCO. An ARMA model is constructed - using a discrete dynamic system - in a difference equation form able for testing stability, and in a matrix form for applying control techniques. Since relative gains provide a useful measure of interaction indices, so relative gain matrix procedure is followed for modifying the interconnected static gains through introducing computing relays with adjustable gains in the open loop control system for ensuring composite system stability.

Pole assignment technique is used for designing the suitable closed-loop strategy for composite system. Numerical results agree with the effectiveness of both of the suggested interconnected computing relays and the designed control strategy.

INTRODUCTION:

In a previous work $\{9\}$, modelling and simulation for multivariable chemical system in Semadco Urea-plant were presented. The simulated system is the High Pressure Boiler Feed Water Heater (HP-BFW-E127), which governs the inlet temperature of ammonia converter R-107.

Based Upon practical knowledge, experimental investigations and mathematical simulation techniques, multivariable interconnected dynamic model is constructed as shown in figure (1) (without the double circled elements). Now, to accomplish the job of designing appropriate control technique for governing and modifying the system performance, reformulation of the deduced model in a suitable form for applying control methods on multivariable interconnected system is necessary. Afterwords, deduction of proper interaction between input / output channels represents a next step. Thus, this work is consisting from the following main three parts:

1- Discretization and ARMA Model construction:

Discrete model is a suitable form for computer applications. Several methods can be used for representing the corresponding diference equations or discrete transfer functions [3, 6, 8, 10, 12]. The ARMA model [4, 5] representation is a suitable and efficient one for testing linearized multivariable systems. So, We follow this representation for constructing our physical model in a suitable form for applying control strategies.

2- Interconnected system stability:

Interaction between control loops is a significant factor affecting the goodness and stability of complete system. Interaction conditions make different loops to help; or to fight each other. In other words, regulating action for some control loops may de-regulate and disturb the outputs of the other loops. So, system is said to be fully coupled if interaction improves stability. The relative gain matrix procedure [1,2] provides a useful technique for testing and then ensuring the interconnected stability conditions for the open loop system, that is by designing suitable interconnection modification factors.

3- Pole Assignment control strategy:

The pole placement [10,11] is one of the simplest direct design procedures. For which, the key idea is to find a feedback law such that the closed loop poles have the desired locations. The classical pole-assignment method [11] does not require that the interaction matrix to be minimum phase, and makes no constraints upon the channel time delays. So, it is a proper choice for obtaining control law for the practical chemical system under investigation. In order to apply this technique, the mathematical model has to be presented in a form suitable for computer control application as follows:

I- DISCRETIZATION AND ARMA MODEL CONSTRUCTION:

The pulse transfer function is H * Gp(z) (the hold element and the process), and can be related to the continuous transfer functions of hold H(s) and Gp(s) by a proper choice of T [4,5]. For the physical system of figure (1) with T = 0.5 sec. and $\Delta = 1.05$, we have [7]:

wintering intings backlast and ins system with

E.2 🖌

MANSOURA ENGINEERING JOURNAL (MEJ) VOL. 19, NO. 2, JUNE 1994 E. 3

$$H G_{v1}(Z^{-1}) = \frac{0.004 Z^{-1}}{1 - 0.87 Z^{-1}}$$
 (1-a)

$$H G_{v2}(Z^{-1}) = \frac{0.0021 Z^{-1}}{1 - 0.87 Z^{-1}}$$
(1-b)

$$H G_{p31}(Z^{-1}) = \frac{Z^{-2} (-0.000242 Z^{-1})}{(1-0.999 Z^{-1})}$$
(1-c)

$$H G_{p32}(Z^{-1}) = \frac{Z^{-2} (-0.000181 Z^{-1})}{(1-0.999 Z^{-1})}$$
(1-d)

$$H G_{p33}^{(Z^{-1})} = \frac{Z^{-2} (-0.008 Z^{-1})}{(1 - 0.999 Z^{-1})}$$
(1-e)

For general interconnected multivariable system, a process model is given by:

$$Y(t) = \frac{B(s)}{A(s)} U(t-\Delta) + d(t)$$
(2)

where : A is the time delay

d(t) is a disturbance, and it may be: a- control value b- slowly varying value c- fed through a feed forward element d- stocastic signal The discrete time equivalent of equation (2) is given as:

$$Y(t) = \frac{B(Z^{-1})}{A(Z^{-1})}U(t-k) + D(z)$$
(3)

or written in an ARMA Model form as [3, 8, 10]:

$$A(Z^{-1}) Y(k) = Z^{-k} B(Z^{-1}) U(k) + D(k)$$
(4)

where $A(Z^{-1})$ and $B(Z^{-1})$ are polynomials of orders n_a and n_b respectively, and D(k) is the disturbance model. Substitution of system equations (1-a) to (1-e) into equation (4), produces the following ARMA model representation of our plant, with Y₂(k) is the disturbanc/ channel:

$$Y_{1}(k) = -a_{1}Y_{1}(k-1) + b_{1}U_{1}(k-1) + b_{2}U_{2}(k-1)$$
(5)

$$Y_{2}(k) = -a_{2}Y_{2}(k-1) + b_{3}U_{1}(k-1) + b_{4}U_{2}(k-1)$$
(6)

E.H. EL-KONAYALY, K.M. SOLIMAN & N. MEEKAWY

$$Y_{3}(k) = -a_{3}Y_{3}(k-1) - a_{4}Y_{3}(k-2) + b_{5}U_{1}(k-4) + b_{6}U_{2}(k-4) + b_{7}U_{3}(k-1) + b_{8}U_{3}(k-4)$$
(7)

where : $a_1 = -0.87$, $b_1 = 0.004$, $b_2 = -0.968 * 10^{-6}$ $a_2 = -0.87$, $b_2 = 0.0021$, $b_4 = -0.38 * 10^{-6}$ $a_3 = -1.869$, $b_3 = 0.00036$, $b_7 = 0.008$ $a_{a} = 0.869$, $b_{a} = 0.0021$, $b_{g} = -0.00696$

Since Y (k) represents the disturbance, the following assumptions are considered acceptable [5, 7]:

$$Y_{3}(k-2) = Y_{3}(k-1) , \qquad U_{1}(k-4) = U_{1}(k-1) U_{2}(k-4) = U_{2}(k-2) , \qquad U_{3}(k-4) = U_{3}(k-3) = U_{3}(k-1)$$

and substituting:

 $a_5 = a_3 + a_4 = -1$, $b_9 = b_7 + b_8 = 0.00104$ The ARMA model will be:

$$\begin{bmatrix} Y_{1}(k) \\ Y_{2}(k) \\ Y_{3}(k) \end{bmatrix} = -\begin{bmatrix} a_{1} & 0 & 0 \\ 0 & a_{2} & 0 \\ 0 & 0 & a_{3} \end{bmatrix} \begin{bmatrix} Y_{1}(k-1) \\ Y_{2}(k-1) \\ Y_{3}(k-1) \end{bmatrix} + \begin{bmatrix} b_{1} & b_{2} & 0 \\ b_{3} & b_{4} & 0 \\ b_{5} & b_{6} & b_{9} \end{bmatrix} \begin{bmatrix} U_{1}(k-1) \\ U_{2}(k-1) \\ U_{3}(k-1) \end{bmatrix}$$
(8)

where the interaction matrix is:



Through which, the overall interconnected open loop stability can be decided when all roots of the characteristic equation :

E.4

|ZI-B| = 0 lie inside the unit circle disk.

For our system, the calculated roots are:

$$\begin{bmatrix} z_1 & z_2 & z_3 \end{bmatrix} = \begin{bmatrix} 0.00104 & 0.00434 & 0.00176 \end{bmatrix}$$

Although these roots tell us that, the overall interconnected system have to be highly stable, their approximate zero values represent dead-bent operations, which may produce contracted and unrelaxed performance pushing the system to instability, that is due to weak and unsuitable interconnections.

Truly, when this system is used for applying control techniques, results show diverging unstable response. so, the following section presents detailed study about the interconnected system stability conditions, with designing proper interconnection factors to convert the original open loop system to more reliable one suitable for applying differential control techniques.

II_INTERCONNECTED SYSTEM STABILITY:

The relative gain matrix procedure [1,2] used for testing, and then accomplishing the interconnected stability conditions is carried out in the following steps:

1- Constructing the interconnected multivariable system input- output relationship in the form:

$$Y_{j}(s) = \sum_{j=1}^{n} G_{ij}(s) U_{j}(s), i=1,2,...,n$$
 (10)

where G is the T.F between input j and output i,

n is the system order

2- Determining the steady state gain matrix (S.S.G.M.):

$$K = \begin{bmatrix} K_{ij} \end{bmatrix} , K_{ij} = \frac{\delta Y_i}{\delta U_j} \Big|_{U_i = \text{ constant }, 1 \neq j}$$
(11)

Where : K is the open loop static gain when all other manipulated variables are kept constant.

Applying for our practical system (Figure (1) but without the double circled gains), the S.S.G.M. will be:

	0.031	0.0164	0	ļ
K az	0.0093	0.0164	0	
	-0.0075	-0.00297	8	

- Converting equation (10) to relate the deviations between variables:

$$\Delta Y_{i} = \sum_{j=1}^{n} K_{ij} \Delta U_{j}$$
, $i = 1, 2, ..., n$ (12)

4- Calculating gain for each loop when all other loops are closed, and all other controlled variables are returned to their set points:

$$K'_{ij} = \frac{\Delta Y_i}{\Delta u_j} \bigg| \Delta Y_i = 0, 1 \neq j$$
(13)

As functions of K_{ij} , complicated expressions for K_{ij} are deduced for the general 3-dimensional case [7]. These expressions are much simplified when applying for our real system having $K_{13} = K_{23} = 0$:

Thus: $K' = \begin{bmatrix} 0.0217 & -0.03827 & \infty \\ -0.0217 & 0.01148 & \infty \\ \infty & \infty & 8 \end{bmatrix}$

5- Computing relative gain matrix (R. G. M.) μ , Where:

$$\mu = \left[\mu_{ij} \right] , \quad \mu_{ij} = k_{ij} \neq K'_{ij}$$
(15)

MANSALINA ENGLISHER SUL ALLENAL LADO / TODO	MANGOURA	ENGTNEERING	TOURNAL	1	MEJ	>	VOL.	19,	NO.	2,	JUNE	1994	L.,	1
---	----------	-------------	---------	---	-----	---	------	-----	-----	----	------	------	-----	---

F 7

		1.4286	-J. 4286	ر ہ
producing	μ =	-0.4286	1.4256	0
		0	0	1

5- For stable interconnected system, the following properties must be fulfilled for the R.G.M.:

i- ∑ elements in any row or any column =1

- 11- μ_{ij} must be positive, since negative values mean negative interactions, i.e. undesirable system from control point of view because loops fight each other.
- ili- $\mu_{ij} = 1$ means no interaction, and amount of deviation from unity represents amount of stability combination between controlled and

manipulated variables.

Accordingly, it is clear that our original system is completely unstable one. Hence, design of computing - or blasing - relays which can be done easily from practical point of view, is a good idea for solving this problem. On the other side, it is notable that the only way for choosing the rates of these relays is long and unguaranteed trial and error prone.

As a final result for several trials, the chosen computing relays shown in figure (1) by double circled elements are tested and ensured to fulfil the necessary stability conditions. For this choice:

		3.1	4.92	0]
Kmodified	¥	-1.86	4.92	0
		-75.02	-383.76	2000
		4.95	13.12	∞]
Kmodifed	,	-4.96	7.872	e
		a	-383.76	2000
		0.625	0.375	٥٦
F modified	=	0.375	0.625	0
		0	0	1

These results represent perfectly stable interconnected modified system. Resubstitution in the steps of deducing ARMA model produces the following modified interaction matrix:

	0.4	0.63	0]
$F(z^{-1}) =$	-0.072	0.63	0
	~0.00968	-0.0491	0.26

fdr which, roots of characteristic equation will be:

 $\begin{bmatrix} Z_1, Z_2, Z_3 \end{bmatrix} = \begin{bmatrix} 0.26, 0.515+j0.1794, 0.515-j0.1794 \end{bmatrix}$

Telling us that, this chosen modification satisfies reliable uncontracted stability conditions for the interconnected ARMA model.

IIL-POLE ASSIGNMENT SELF TUNING CONTROLLER:

An initial stage in multivariable design is to deduce interaction between input-output channels by self tuning on-line computer aided synthesis method [4,10,11]. The self tuning on-line nature requires intutive engineering judgements concerning sample rate, slew limiting and many other factors which are parts and parcel of digital controller implementation.

The pole placement technique [11] is one of the simplest direct self tuning design procedures. The key idea of this technique is to find a feedback law such that, the closed loop poles have the desired locations. The classical pole assignment method does not require that $B(Z^{-1})$ is minimum phase, and makes no constraints upon the channel time delay. Thus, it is a preferable technique for controlling our chemical process. For the general form of disturbed multivariable system:

$$\left[I + A(z^{-1})\right] Y(t) = Z B(z^{-1}) U(t) + \left[I + C(Z^{-1})\right] e(t)$$
(16)

Where the noise corrupting the system e(t) is such that $(I + C(Z^{-1}))$ is inverse stable. To avoid restriction on B(z^{-1}), we choose the following control law:

$$\left[I + F(z^{-1})\right] U(t) = -G(z^{-1}) Y(t)$$
(17)

where : $G(Z^{-1}) = G_0 + G_1 Z^{-1} + \dots + G_{ng} Z^{-ng}$ $F(Z^{-1}) = f_1 Z^{-1} + \dots + f_{nf} Z^{-nf}$

F, and G, are $p \times p$ coefficient matrices,

 $n_{f} = n_{h} - 1$, $n_{f} = n_{h} + k - 1$

Shifting closed loop poles to the location (assigned poles) defined by the polynomial matrix [$1 + T(z^{-1})$], i.e.:

$$\psi(t) = [I + F(z^{-1})] [I + T(z^{-1})]^{-1} e(t)$$
 (18)

where $n \leq n + n + k - 1 - n$

Substituting equations (17) and (18) into equation (16) producing:

$$\begin{bmatrix} I + A(z^{-1}) \end{bmatrix} \begin{bmatrix} I + F(z^{-1}) \end{bmatrix} + Z^{-k} B(z^{-1}) G(z^{-1}) = \\ \begin{bmatrix} I + C(z^{-1}) \end{bmatrix} \begin{bmatrix} I + T(z^{-1}) \end{bmatrix}$$
(19)

from which, control parameters can be calculated by equating coefficients of similar powers of (Z^{-1}). Thus, the calculation procedure can be summarized in the following steps:

1- Reconstructing equation (16) to the form:

$$Y(t) = -A_{1} Y(t-1) - \dots -A_{na} Y(t-n_{a}) + B_{o} U(t-k) + \dots + B_{nb} U(t-k+n_{b}) + C_{1} e(t-1) + \dots + C_{nc} e(t-n_{c})$$
(20)

and using Recursive Least Square (RLS) (7) method, estimated parameters \hat{A} and \hat{B} can be calculated.

- 2- Given A and B and pre-specified T, estimated G and f can be calculated by solving equation (19) at each sample.
- 3- Y(t) can be calculated from equation (18).
- 4- Control law U(t) is calculated from equation (17). It is notable that, for non zero reference signals, Y(t) is replaced by [$Y(t) - Y_r(t)$] where $Y_r(t)$ is p-vector of nominally constant reference demand.

This procedure is applied on our modified interconnected ARMA model with substituting:

Setting values: $Y_{r1} = 0.7$, $Y_{r2} = 0.65$, $Y_{r3} = 0.8$ change in each set point = (0.05 or -0.05)

R. L. S. : Forgetting factor $\lambda = 0.99$

Covariance matrix element p = 108

Noise levels e (t) changes from -0.15 to 0.0004

- e_(t) changes from -0.15 to 0.0005
- e_(t) changes from -0.15 to 0.0006

Figures (2), (3) and (4) γ samples of the obtained control performances,

which prove that the pole assignment controller has been succeded for: a) Regulating the system response, and keeping it equal to the reference signal variations for all the chosen poles locations (0.1 to 0.85).

b) The controller could reject random disturbances which corrupt the system output.

the second program in the second seco

CONCLUSION: :

Multivariable control strategy is designed for controlling performance of interconnected system which simulates a real chemical process in SEMADCO Urea- plant. Open loop system stability is ensured by designing appropriate computing relays for modifying the different interconnected static gains. Relative gain matrix procedure is used for this purpose.

the instantion of the second states of the second second

On the other hand, closed loop controllers for the composite system are designed by using pole assignment technique. Good results are obtained which agree with the effectiveness of the designed control strategy.

REFERENCES:

- 1- Bristol E.H., "Cn a new measure of interaction for multivariable process control", IEE, Aut. Cont., [1966].
- 2- Carlos A. Simth and Armando B. Corripio, " Principles and practice of Aut. Process control", John Willy & sons., [1985].
- 3- Clark D. W., "Introduction to self-tuning theory and applications", IEEE cont. Eng., series 15, [1985].
- 4- A.M. Ferreira, I. J. Barker, and I. M. Maclead, "An Application of Multivariable self-tuning control", IEE, Aut. Cont., Series 15, [1985].
- 5- George Stephanopoulos, " Chemical Process Control-an Introduction to theory and practice", prentice Hall Int. Inc. [1984].
 - 6- IFAC 7-th conference on Digital computers Applications to process control, Sept. [1985].
 - 7- N. Mekkawy, "Multivariables Control Systems", B.Sc Thesis, Mansoura University, [1993].
 - 8- A.J. Morris, Y. Nazer and R.K. Wood, "Single and Multivariable application", IEE Aut. Control, Series 15, [1985].
 - 9- K.M. Soliman and N. Mekkawy," Modeling and simulation for multivariable chemical system in SEMADCO UREA - Plant," Mansoura Eng., Journal, Vol. 16, No. 1, June [1991].
 - 10- P.E. Wellstead and D.L. Prager, "Self Tuning Multivariable Regulators", IEE Control Eng. Series 15, [1985].

11- P.E. Wellestead and M.B. Zarrop, "Self-Tuning systems and signal Processing", John wiley & Sons. Ltd, [1991].

al Regulating the Colter responses and responses it equil to reference the equilations of the content of the sections of the section of the s

THE COLOR OF THE







Block diagram of multivariable interconnected Aomina converter

system with HP-PFW heater.

$$G_{v1} = 0.031/(3.6 \text{ s}+1) , G_{v2} = 0.0164/(3.6 \text{ s}+1) ,$$

$$G_{p31} = -0.242 \cdot \exp(-1.05 \text{ s})/(600 \text{ s}+1) ,$$

$$G_{p32} = -0.181 \cdot \exp(-1.05 \text{ s})/(600 \text{ s}+1) ,$$

$$G_{p33} = 8.0 \cdot \exp(-1.05 \text{ s})/(600 \text{ s}+1) ,$$





17127.4

First Uase : Poles arc +0.3 , +0.2 , +0.1



Fig(3)

Second Case : Poles are +0.7, +0.6, +0.5



Fig(4)