

12-6-2020

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Eid, El-Desouki (2020) "Natural Convection Heat Transfer between Two Concentric and Eccentric Oblate Hemi Spheroids with Different Elliptical Ratios.," *Mansoura Engineering Journal*: Vol. 33 : Iss. 4 , Article 6. Available at: <https://doi.org/10.21608/bfemu.2020.127842>

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NATURAL CONVECTION HEAT TRANSFER BETWEEN TWO CONCENTRIC AND ECCENTRIC OBLATE HEMI SPHEROIDS WITH DIFFERENT ELLIPTICAL RATIOS

انتقال الحرارة بالحمل الطبيعي بين نصفي بيضاوي متقارب أفقياً متمركزين وغير متمركزين لهما نمبة أهليل متغيرة

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ملخص

في هذا البحث يتم دراسة انتقال الحرارة بالحمل الطبيعي بين نصفي بيضاوي متقارب أفقياً متمركزين وغير متمركزين لهما نمبة أهليل متغيرة عملياً وعددياً. تم تصنيع عدد أربعة أزواج من نصفي البيضاوي، كل زوج منهم له نمبة قطر تساوي 2، والأربعة أزواج لهم نسب أهليل (صفر، 0.25، 0.5، 0.75) باستخدام ماكينة قطع سلبي مبرمجة. تم تسخين نصف البيضاوي الصغير بينما يتعرض نظيره الكبير إلى درجة حرارة الغرفة حيث يتم انتقال الحرارة بالحمل الطبيعي بينهما عبر الحيز الهوائي. تناولت الدراسة العملية اختيار كل زوج في أوضاع مختلفة (أفقياً - مائلاً - رأسياً - مائلاً ومرفقاً - رأسياً ومرفقاً). تم عمل محاكاة نظرية لدراسة تأثير اللامركزية بين نصفي البيضاوي وذلك عن طريق وضع المعادلات الحاكمة لسريان تبادلي انضغاطي مستقر ثلاثي البعد خلال الحيز البيضاوي وقد تم حل هذه المعادلات عددياً باستخدام برنامج معد خصيصاً للحل العددي لديناميكا الموائع FLUENT-CFD كما تم التحقق من صلاحية نتائج التحليل النظري عن طريق مقارنة بعضها بنظائرها العملية. هذا وقد أوضح التحليل النظري تفاصيل الحركة الحلقية للهواء في الحيز بين نصفي البيضاوي. تم صياغة معادلات وضعية نصف نتائج هذا البحث العملية والنظرية بانحراف في حدود 10%. وقد استقرت مقارنة نتائج هذا البحث بنظائرها العملية والنظرية بين نصفي كرتين إلى أن انتقال الحرارة بين نصفي بيضاوي يتحسن بزيادة نسبة الأهليل. كما يتحسن انتقال الحرارة بالحمل الطبيعي باللامركزية الرأسية الموجبة عن المركزية واللامركزية الرأسية السالبة.

ABSTRACT

In this paper, the natural convection heat transfer between a pair of concentric and eccentric oblate hemi-spheroids with different elliptical ratios was depicted experimentally and numerically. Four pairs of oblate hemi-spheroids having elliptical ratios of 0.0, 0.25, 0.5, 0.75 and a diameter ratio of 2 for each pair were cut using the wire-cut JSEDM CNC machining. The inner hemi-spheroid was heated while the outer one was exposed to the room temperature. The experimental tests scan the effect of the orientation modes (horizontal, inclined, vertical inclined revolved and vertical revolved) on the natural convection heat transfer between the inner and outer surfaces of each pair. A mathematical model was devoted for the case study to investigate the effect of the eccentricity on the thermal performance of such cases. The model was solved numerically using FLUENT CFD solver. The CFD results were validated via corresponding experimental data. The temperature and velocity contours of the air gap were displayed to indicate the ring movement of the buoyancy driven air plume. The comparison among the results of the present attempt and those by the literature implied that; a notable increase in the natural convection heat transfer rates could be satisfied through the gaps among successive layers of hemi-spheroids having higher elliptical ratio rather than the hemi-spherical ones. Also, the positive vertical eccentricity shows remarked increase in natural convection heat transfer rates rather than both concentric and negative eccentric cases.

KEY WORDS: *Natural Convection, Heat Transfer, Spheroids, Elliptical ratio, Orientation mode, CFD solvers.*

INTRODUCTION

Hemi-spheres and hemi-spheroids become popular in modern glazed buildings. Glazed buildings are useful in bringing daylight and solar heat to indoor space. For hemi-spheroids of multiple layers with different elliptical ratio, the natural convection heat transfer among these layers is often important in various applications such as; nuclear reactor design, aircraft cabin insulation, cooling of electronic equipments, thermal storage systems, solar energy collectors, heating heads of Stirling machines, geophysical fields and eggs-white shell bodies. The present attempt aims at an adequate evaluation for the thermal performance of such applications that concerning natural convection heat transfer. An experimental investigation concerning natural convection heat transfer through air enclosed between two isothermal concentric spheres of various diameter ratios ranging from 1.19 to 3.14 at $2 \times 10^4 \leq Gr \leq 3.6 \times 10^6$ was provided by [1]. Nusselt-Grashof correlations were presented for the measured heat-transfer data for four different diameter ratios and the correlation fitting was within 15.5 % deviation. Another experimental investigation concerns natural convection heat transfer between two isothermal concentric spheres of various diameter ratios ranging from 1.09 to 2.81 with water, two silicon oils yielding $4.7 \leq Pr \leq 4148$ and $1.3 \times 10^2 \leq Ra \leq 5.8 \times 10^8$ was provided by [2]. A $(k_{eff}/k) - Ra$ heat transfer correlation was presented for each of the three fluids individually within 13.4% deviation. A finite-difference solution for steady natural convective flow in a concentric spherical annulus with isothermal walls had been obtained by [3]. Results were presented for a diameter ratios of 2 and 3, Prandtl numbers of 0.02, 0.7 and 6 and $10^2 \leq Ra \leq 10^6$. Excellent agreement with previous experimental data was obtained. The transient laminar natural convection heat transfer of fluids between two concentric isothermal spheres was investigated theoretically by [4]. The fluids were assumed

to be initially at rest and then the inner wall is subjected to a step change of temperature. The transient behavior of the flow field and the temperature distribution at different Rayleigh numbers and radius ratios were analyzed by finite difference methods. The results showed that the Rayleigh number and radius ratio have a profound influence on the temperature and flow fields. A transient analysis had been investigated numerically to determine the heat transfer by natural convection between two concentric spheres with isothermal boundary conditions by [5]. The inner and outer spheres were heated and cooled in a step-wise change of temperature. The analysis lets $10^3 \leq Ra \leq 10^5$, $Pr = 0.7$ and a radius ratio of 2. The computations delivered general $Nu - Ra$ correlations. A numerical study on the heat transfer by laminar natural convection within multi-layer domes with uniform spacing heated from the outside was done by [6]. The flow and temperature fields within the domed enclosure were obtained. Correlations for the heat transfer as a function of the dome shape and gap spacing among the layers were developed. The results showed that the convective heat transfer for fully hemi-spherical domes is 13% higher than that for low profile domes (caps) with small gap spacing and it increases for large gap spacing. The transient temperature and velocity profiles during thermal processes of egg shell bodies filled with a viscous liquid had been studied by [7]. Sodium carboxyl-methyl cellulose suspension was used as a fluid. It has properties similar to egg white shell. The partial differential equations governing the natural convection in a three-dimensional geometry were solved with the computational fluid dynamic FLUENT package. It was observed that natural convection tends to force the slowest heating zone towards the bottom of the egg. The transient natural convection heat transfer had been analyzed for viscous fluids ($Pr = 158, 405$ and 720) in a spherical annulus, with $5 \times 10^3 \leq Ra \leq 6.5 \times 10^4$ and a radius ratio of 2.0 by [8]. Another transient natural convection analysis between concentric spheres having a radius ratio of 2

at $10^3 \leq Ra \leq 5 \times 10^5$ through micro-polar fluids (micro polar parameter is k/μ , $1 \leq k/\mu \leq 5$) had been investigated numerically by [9]. The results showed that the filling of a cavity with a micro polar fluid will improve the thermal energy storage performance because it keeps warmer than the one filled with Newtonian fluid. The effects of height and radius ratios (HR and PR , $HR = H_{cylinder} / r_{sphere}$ and $PR = r_{cylinder} / r_{sphere}$) had been investigated numerically to determine heat transfer by natural convection between a sphere and vertical cylinder with isothermal boundary conditions, [10]. The inner sphere and outer vertical cylinder were heated and cooled in a step-wise change of temperature. The study delivered out empirical collations for a range of $10^3 \leq Ra \leq 10^6$ and $1.2 \leq HR = PR \leq 5$.

The purpose of the current investigation is to depict experimentally the effect of the elliptical ratio of hemi-spheroids on the natural convection heat transfer between a pair of them. The elliptical ratio of the hemi-spheroid was changed four times (0, 0.25, 0.5 and 0.75). Also, the present work investigated experimentally the effect of the orientation modes (horizontal, vertical, inclined, inclined revolved and vertical revolved) on the natural convection heat transfer. Empirical correlations were devoted to describe the experimental results. The present study presents also the effect of both positive and negative vertical eccentricity on the natural convection heat transfer by using a mathematical model. The model was solved numerically using the FLUENT CFD package. Verification of both experimental and numerical results was done to validate the numerical model. Comparisons were attempted among the results of the present work and those by the literature.

EXPERIMENTAL WORK

Referring to figure (1), the meridian planner ellipse has a major axis a and a minor one b . Oblate spheroid is the surface created by rotating the meridian ellipse about the major axis, If $b < a$, the spheroid is called oblate and if $b > a$, the spheroid is called

prolate. The surface equation of the oblate spheroid is, [11]:

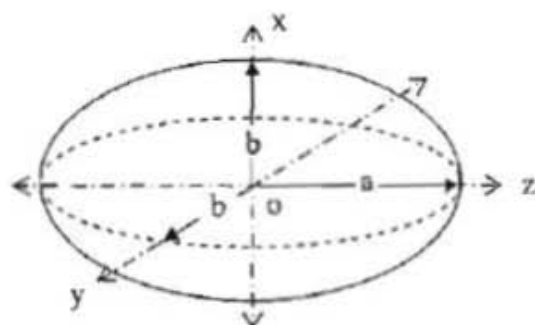


Figure (1), Geometry of the oblate spheroid.

$$\frac{x^2 + y^2}{b^2} + \frac{z^2}{a^2} = 1 \quad (1)$$

The elliptical ratio of the spheroid is:

$$\zeta = \sqrt{1 - \frac{b^2}{a^2}} \quad (2)$$

The surface area of the spheroid is:

$$A = 2\pi a^2 + \pi \frac{b^2}{\zeta} \ln \left(\frac{1+\zeta}{1-\zeta} \right) \quad (3)$$

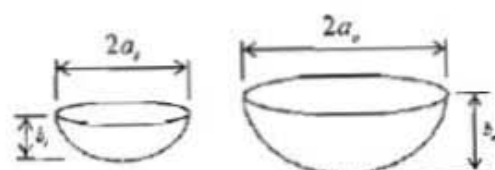


Figure (2), Pair of the hemi-spheroid.

Referring to figure (2), the dimensions and the elliptical ratio of the four tested pairs are listed in table (1).

Table (1), Dimensions of test specimens.

Pair No.	Dimensions in cm.				Elliptical ratio, ζ
	a_s	b_s	a_o	b_o	
I	7.50	7.50	15.00	15.00	0.00
II	7.50	7.26	15.00	14.52	0.25
III	7.50	6.50	15.00	13.00	0.50
IV	7.50	4.96	15.00	9.92	0.75

The wall thickness of each hemi-spheroid is 2.5 mm. Also, the given dimensions are the inner dimensions of the large hemi-spheroid and outer ones for the small one. The four pairs were cut from pure aluminum by using the wire-cut JSEDM CNC machining, [12]. Referring to figure (3), the inner hemi-spheroid was internally heated by an electric

nickel-chrome heater which was buried inside a typical small bakelite hemi-spheroid.

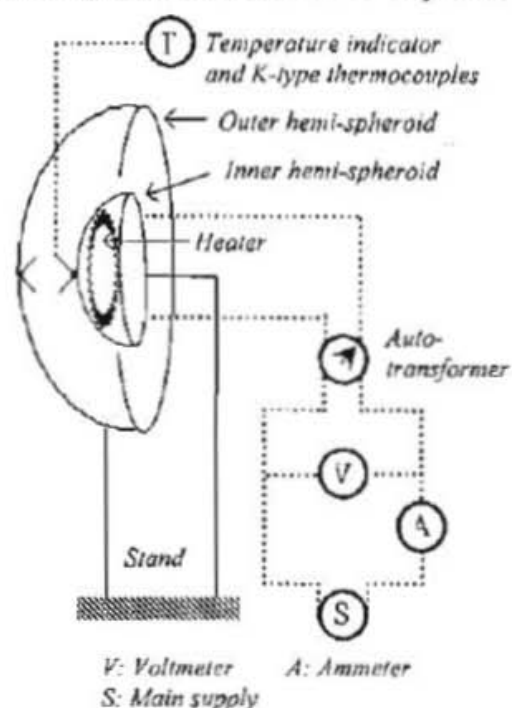


Figure (3), Main parts of the experimental test rig.

An electric insulation tape was covered the heater. The space between the heater and the inner surface of the small hemi-spheroid was filled with dry sand to avoid the convection currents and to sustain an almost uniform heat flux. Also, an asbestos layer having 1.0cm thick was located at the flat end of the small hemi-spheroid to reduce the losses by conduction. Three *K-type* thermocouples were used to measure the temperature of the outer surface of the small hemi-spheroid. Five ones were used to measure the temperature of the inner surface of the large hemi-spheroid. Three ones were used to measure the temperature of the air gap between the two hemi-spheroids. Two ones measure the temperatures of both sides of the asbestos layer. One thermocouple was used to measure the room temperature of a closed laboratory. A digital temperature indicator having a resolution of 0.1°C was used to record the temperatures. The electric power consumed by the heater was controlled by an altering variance unit of 3000 VA capacity. An ammeter of 0.01A resolution and a

voltmeter of 0.1V resolution were used to measure the electric power consumed by the heater, [13]. The experimental work scans the effects of elliptical ratio, orientation modes (vertical, horizontal, inclined, inclined revolved and vertical revolved) as shown in Figure (4), on the natural convection heat transfer between a pair of concentric hemi-spheroids.

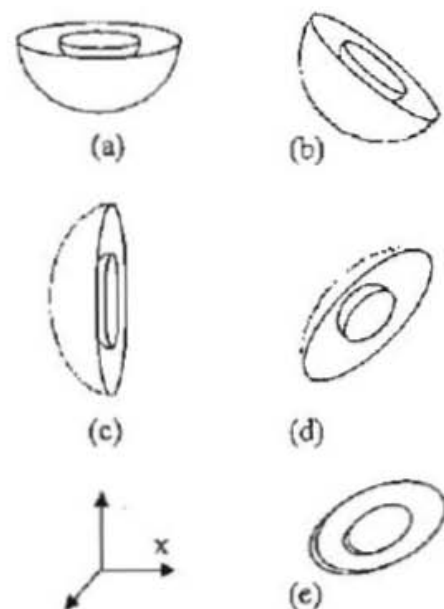


Figure (4), Orientations of the test specimen; (a) Horizontal; ($\phi = 0^\circ$, $\varphi = 0^\circ$), (b) Inclined; ($\phi = 45^\circ$, $\varphi = 0^\circ$), (c) Vertical; ($\phi = 90^\circ$, $\varphi = 0^\circ$), (d) Vertical revolved; ($\phi = 0^\circ$, $\varphi = 90^\circ$), and (e) Inclined revolved; ($\phi = 0^\circ$, $\varphi = 45^\circ$).

EXPERIMENTAL DATA REDUCTION

The main objective of this paper is to provide evidences about the parameters that create a stronger buoyancy-driven plume which results in higher heat transfer coefficient by natural convection in a space between a pair of concentric oblate hemi-spheroids having different elliptical ratios if they were oriented at different orientation modes. The heat transfer by natural convection can be evaluated as follows, [14 and 15]:

$$Q_{\text{convection}} = Q_{\text{total}} - Q_{\text{radiation}} - Q_{\text{conduction}} \quad (4)$$

Where; Q_{total} is the electrical power converted to heat by the electric heater. The

heat transfer by radiation from inner surface to outer one and to air can be found as follows:

$$Q_{\text{radiation}} = \frac{\sigma A_i (T_i^4 - T_o^4)}{\left(\frac{1}{\varepsilon_i} + \frac{(1 - \varepsilon_o)}{\varepsilon_o}\right) \frac{A_i}{A_o}} + \frac{\sigma \varepsilon_i A_i (T_i^4 - T_o^4)}{1 + \varepsilon_i \left(\frac{A_i}{\pi(a_o b_o - a_i b_i)} - 1\right)} \quad (5)$$

The heat transfer by conduction from the asbestos layer covering the flat end of the small hemi-spheroid is as follows:

$$Q_{\text{conduction}} = \frac{\pi a_i b_i (T_{a,i} - T_{a,o})}{\delta_a / k_a} \quad (6)$$

The average convective heat transfer coefficient, average Nusselt number and Rayleigh number can be found as follows:

$$\bar{h}_a = Q_{\text{convection}} / A_i (T_i - T_o) \quad (7)$$

$$\overline{Nu}_a = \frac{\bar{h}_a \ell}{k_a} \quad \text{where; } \ell = b_o - b_i \quad (8)$$

$$Ra_a = \frac{g \beta (T_i - T_o) \ell^3}{\nu_a \alpha_a} \quad (9)$$

The air properties in the above equations are evaluated at the mean temperature, [16 and 17], $[T_m = (T_i + T_o) / 2]$.

MATHEMATICAL MODEL

The partial differential equations governing the air motion in a three-dimensional space due to natural convection heat transfer between a pair of hemi-spheres are the mass, momentum and energy equations. In case of an incompressible fluid flow having constant thermal and physical properties, except for Boussinesq approximation for density in the buoyancy term in momentum equation, these equations could be reduced in Cartesian coordinates as follows, [7]:

$$\text{Continuity equation: } \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad (10)$$

Momentum equation in x-direction:

$$\rho \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = -\frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) \quad (11)$$

Momentum equation in y-direction:

$$\rho \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = -\frac{\partial p}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right) + \rho g \quad (12)$$

Momentum equation in z-direction:

$$\rho \left(u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = -\frac{\partial p}{\partial z} + \mu \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right) \quad (13)$$

Energy equation:

$$\rho C_p \left(u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} + w \frac{\partial T}{\partial z} \right) = \left(u \frac{\partial p}{\partial x} + v \frac{\partial p}{\partial y} + w \frac{\partial p}{\partial z} \right) - \left(\frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z} \right) + k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) \quad (14)$$

This model is provided to study the effect of the eccentricity between a pair of hemi-spheres on the natural convection heat transfer between them; when they were oriented in vertical positions as show in figure (5).

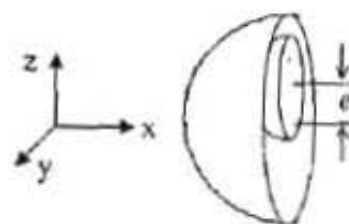


Figure (5). Two-eccentric hemi-spheres.

The boundary conditions for this model are:

$$\text{- At the surface of the inner hemi-sphere; } u = v = w = 0, \quad q = \text{const.} \quad (15)$$

$$\text{- At the surface of the outer hemi-sphere; } u = v = w = 0; \quad T = T_o \quad (16)$$

- At the symmetry plane, $y = 0$

$$\frac{\partial u}{\partial y} = \frac{\partial T}{\partial y} = \frac{\partial v}{\partial y} = \frac{\partial w}{\partial y} = 0 \quad (17)$$

These governing equations are solved numerically using CFD FLUENT, [18 and 19]. The case study was drawn in Gambit and tetrahedral grids with small interval size were created and the previous boundary conditions were defined. This model was exported to the FLUENT CFD solver. The variation of the thermal properties of air with its temperature was taken into consideration to be piecewise polynomials. A segregated, implicit, 3-D, cell-based solver was defined. The gravity effect was considered. The CFD solver makes a number of iterations until the solution is converged. The numerical solution studied the effect of both positive and negative eccentricities;

RESULTS AND DISCUSSION

The transition from conduction to convection regime between two concentric spheres ends at $Ra = 10^5$, [5]. In the present work, all tests were done for $Ra \geq 1.34 \times 10^5$; therefore, the heat transfer in the case study falls in the convection regime. Figure (6) shows the average Nusselt number versus Rayleigh number for horizontal orientation mode ($\phi = 0^\circ, \varphi = 0^\circ$), for the four tested pairs. Rayleigh number in the present work was calculated based on the characteristic length $l = b_o - b_i$, this clarifies that why the pair (IV) has lower values of Rayleigh number. From this figure, it is obvious that; at the same Rayleigh number, the pair (IV) shows a notable increase in Nusselt number rather than the other ones. This is due to, the small gap between the inner and outer surface results in an increase in the air velocity due to the relatively high temperature which reduces the air density in such narrow space. And as a consequence, a stronger upward buoyancy-driven plume could be created. In the results of the numerical model, figure (15) shows that; the air velocity is suddenly increase near to the inner surface and hence it reduces more in the gap to its lowest value near the gap center and it increases again to reach to higher value near the outer surface. Thus; the larger gap allows formation of cold air in space around

the gap center. However, narrow gap reduces the formation of cold air and consequently the formed hot air will be driven upward. The same tendency was even more remarked in figures (7, 8, 9 and 10). Figure (11) shows Nusselt number versus Rayleigh number for the tested pair (I), for different orientation modes (horizontal, inclined and vertical). The inclined orientation shows a quite increase in the free convective heat transfer rather than both horizontal and vertical orientation modes. Figure (16) shows the path lines of air in a $y-z$ plane at $x = -1.5$ cm. At the upper half of the inner sphere and due to the high temperature, a high velocity flow is separated from the surface and escaping upward towards the outer surface. When it reaches the inner surface of the outer sphere and due to the low temperature, as shown in figure (17), it directs downward towards the lower half of the outer sphere. This will reduce the buoyancy driven upward plume for the vertical orientation mode. It should be emphasized that; this flow pattern likes the falling vortex-eddy type (postulated flow pattern). This reduction is somehow reduced for the three spheroid pairs as clear in figures (12, 13 and 14).

The previous experimental results were fitted to determine empirical correlations among Nusselt number, Rayleigh number and the elliptical ratio as follows:

$$\bar{Nu} = C (Ra)^n \left(\frac{1}{\zeta} \right)^m \quad (18)$$

For $\begin{cases} 1.34 \times 10^5 \leq Ra \leq 6.32 \times 10^6 \\ 0 < \zeta \leq 0.75 \end{cases}$

Where; the constants C, n and m are tabulated as follows:

Table (2), Constants of the empirical correlations.

Orientation	Constants		Deviation
	C	n	
Horizontal; ($\phi = 0^\circ, \varphi = 0^\circ$)	C	0.2360	±11.7 %
	n	0.2425	
	m	0.1371	
Inclined; ($\phi = 45^\circ, \varphi = 0^\circ$)	C	0.2371	±14.2 %
	n	0.2489	
	m	0.1381	

Vertical; ($\phi = 90^\circ$, $\varphi = 0^\circ$)	C	0.2201	$\pm 13.0\%$
	n	0.2308	
	m	0.2077	
Vertical revolved; ($\phi = 0^\circ$, $\varphi = 90^\circ$)	C	0.2348	$\pm 12.3\%$
	n	0.2349	
	m	0.1506	
Inclined revolved; ($\phi = 0^\circ$, $\varphi = 45^\circ$)	C	0.2628	$\pm 11.8\%$
	n	0.2489	
	m	0.2415	

The numerical results are presented for the case study to investigate the effect of both positive and negative eccentricity for a pair of hemi-spheres having the same dimensions of both ones that were tested experimentally for vertical orientation mode. As the surface areas of the hemi-sphere pair are not equal the non-uniform tetrahedral meshing scheme should be used, figure (18). The CFD model reported the convective heat transfer coefficient which is used in Nusselt number calculations and it also reported the air temperature from its average volume-integral which is used for Rayleigh calculations. The numerical model was validated by comparing its results that were obtained for a pair of concentric hemi-spheres when they oriented vertically with those from the experimental tests. Figure (19) shows a quite agreement between the results of both numerical solution and experimental data. Figure (20) shows the temperature contours on three successive surfaces along x -direction. The temperature of inner hemi-sphere edge is higher than that of the outer hemi-sphere and it is obvious that the upper edge of the inner hemi-sphere has the highest temperature and its lower edge has the lowest temperature and the *v*.s.a versa for air density. Due to the effect of gravity, the air near the surface of inner hemi-sphere flows upward about its surface. The hotter air meets at the top edge of inner hemi-sphere and creates a hot boundary layer. As the inner hemi-sphere surface was kept hotter, the momentum of the created upward buoyant plume keeps the upward air movement to meet the inside surface of outer hemi-sphere. The temperature of outer hemi-sphere is lower, and due to the effect of the convective heat

transfer from the outer surface of the outer hemi-sphere, the air on its inside surface is cooled and its density becomes higher. Thus, the air near the outer hemi-sphere flows downward about its surface. At the steady state, the air reaches the bottom surface of outer sphere and does not rise to form a stagnation zone. Thus, a moving enclosed ring of air will appear as clear in figure (21). Referring to figures (22 and 23), for positive eccentricity ($e = +2.5$ cm or $e/l = +0.3333$) the air has higher temperature at the top edge of the inner hemi-sphere and it has also a quite little temperatures at the bottom edge of the outer hemi-sphere. This produces a quite stronger upward plume rather than that of concentric hemi-spheres. Temperature and velocity magnitude versus y -axis in the meridian ellipse at three local z -levels are clear in figures (24 and 25). Figure (25) shows the highest value of velocity at the top vertex of the inner hemi-sphere and it reduces along the gap distance in y -direction. Such plots may be multifold the stream-vortices formation. For two eccentric hemi-spheres ($e = -2.5$ cm, negative eccentricity), the area above inner sphere is larger and it has a disadvantage of natural convection heat transfer as it is quite cold as shown in figure (26). The velocity of air becomes quite greater at bottom narrow space rather than that at the top wide space as shown in figure (27). Also, a very small stagnation zone was formed at the upper edge of the outer hemi-sphere. Referring to figures (28 and 29), the effect of both positive and negative eccentricities on free convection heat transfer is clear. A correlation among Nusselt number, Rayleigh number and eccentricity was deduced as follows:

$$\overline{Nu} = C (Ra)^n (e/l)^m \text{ For } 10^5 \leq Ra \leq 10^7 \quad (19)$$

Where; the constants C , n and m are tabulated as follows:

Table (3), Constants of the empirical correlation.

Eccentricity	Constants		Deviation
	C	n	
Positive eccentricity	C	0.2201	$\pm 1.3\%$
	n	0.2308	
	m	-0.1085	

Negative eccentricity	C	0.2201	±1.8 %
	n	0.2308	
	m	0.1371	

COMPARISON AMONG PRESENT WORK AND PREVIOUS WORKS

A comparison among the experimental results of the present work and the experimental results of the previous work will be discussed in this section. Another comparison between the numerical predictions of the present work and pre-correlated numerical data in the literature will be also clarified.

An experimental investigation between two concentric spheres of various diameter ratios and $2 \times 10^4 \leq Gr \leq 3.6 \times 10^6$ was provided by [1]. The data were correlated as:

$$\overline{Nu} = 0.332 Gr^{0.27} (\ell/r_i)^{0.517} \quad (20)$$

A CFD solution for natural convective flow in a concentric spherical annulus had been obtained by [3]. Results were presented for a diameter ratio of 2 and 3, Prandtl numbers of 0.02, 0.7 and 6 and $10^2 \leq Ra \leq 10^6$.

An analysis had been investigated numerically to determine the heat transfer by natural convection between concentric spheres by [5], at $Pr = 0.7$ and a radius ratio of 2. The computations were correlated as:

$$\overline{Nu} = 0.21 Ra^{0.24} \quad (21)$$

A numerical study of heat transfer by natural convection within multi-layer domes having uniform spacing was done by [6]. Another study was done by [10] and its predictions were correlated as:

$$\overline{Nu} = 0.206 Ra^{0.28153} \quad (22)$$

The experimental data of [20] were correlated as:

$$\overline{Nu} = 0.74 (1/(1+Pr))^{0.25} (Ra^*)^{0.25} \quad (23)$$

The experimental results of the present work of four pairs of hemi-spheroids having different elliptical ratios when they were oriented as inclined and revolved, i.e. $\phi = 0^\circ$, $\phi = 45^\circ$ were plotted as shown in figure (30). Also, the numerical CFD results for a pair of hemi-spheres when they were

oriented vertically, i.e. $\phi = 90^\circ$, $\phi = 0^\circ$ with positive and negative eccentricities were plotted in the same figure. From this figure, it is clear that, the increase in the elliptical ratio of the hemi-spheroids results in a remarkable increase in the convective heat transfer. In other words, the increase in the elliptical ratio of the oblate successive layers of concentric hemi-spheroids can satisfy higher convective heat transfer rather than those having hemi-spherical surfaces. Also, the comparison among the experimental and CFD results of the present work and those by the literature for the case of natural convection heat transfer between a pair of concentric hemi-spheres shows a notable fairly good agreement.

CONCLUSIONS

This paper reports the results of a study of natural convection heat transfer between pairs of concentric and vertically eccentric hemi-spheroids having a radius ratio of 2.0 with different elliptical ratio (0, 0.25, 0.50 and 0.75). Eight geometrical shapes for four pairs of hemi-spheroid were drawn on a PC and were manufactured by using CNC wire-cut machining. The experimental tests were conducted for each pair such as the inner small hemi-spheroid is heated and the outer one is non-heated and it was exposed to ambient. Each pair of hemi-spheroids was tested experimentally at different orientation mode. A mathematical model was formulated to predict the natural convection of air inside the space between a pair of concentric and either positive eccentric or negative eccentric hemi-spheres. The model was solved numerically using the FLUENT CFD package. The main conclusions of the present work can be summarized as follows:

1. Natural convective heat transfer in the space between two concentric hemi-spheroids can be increased by increasing the elliptical ratio with an approximate percent as follows;

Elliptical ratio, z	0.25	0.50	0.75
Percentage increase in Nu.	8.77%	19.56%	28.77%

- The situation of a pair of hemi-spheroids such as the minor axis of its meridian section is inclined to horizontal plane and the major axis is parallel to the horizontal plane produces stronger buoyancy upward driven plume and resulted in higher free convective heat transfer rates rather than other situations.
- The situation of a pair of hemi-spheroids such as the minor axis of the meridian section is parallel to horizontal plane and the major axis is perpendicular to the horizontal plane resulted in lower free convective heat transfer rates, so, it may be preferred for thermal energy storage applications.
- The validated numerical CFD approach shows that the positive eccentricity results in higher free convective heat transfer rates between a pair of hemi-spheres rather than both concentric and negative eccentric cases.
- The present CFD model can be used to predict the thermal flow characteristics for the case study with different fluids having different Prandtl number.

NOMENCLATURE

Symbol	Description	Unit	Symbol	Description	Unit
A	Surface area	m^2	Q	Heat transfer rate	W
a	Major axis length	m	q	Heat flux	W/m^2
b	Minor axis length	m	Ra	Rayleigh number	
e	Eccentricity	m	Ra^*	$\frac{0.5tRa}{(b_1b_0)^4((b_1)^{-4} + (b_0)^{-4})^2}$	
C	Specific heat	$J/kg.K$	r	Radius	m
g	Gravity acceleration	m/s^2	T	Temperature	K
h	Heat transfer coefficient	$W/m^2.K$	t	Time	s
k	Thermal conductivity	$W/m.K$	ϕ	Angle of inclination of major axis to horizontal.	<i>Degree</i>
u, v, w	Velocity components	m/s	φ	Angle of inclination of minor axis to horizontal	<i>Degree</i>
x, y, z	Cartesian coordinates	m	$\ell = b_o - b_i$	Characteristic length	m
ζ	Elliptical ratio		μ	Dynamic viscosity	$Pa.s$
α	Thermal diffusivity	m^2/s	ν	Kinematical viscosity	m^2/s
β	Volume coefficient of expansion	K^{-1}	ρ	Density	kg/m^3
δ	Thickness	m	σ	Stefan-Boltzman constant	W/m^2K^4
ε	Surface emissivity				
Pr	Prandtl number				
P	Pressure	Pa			

Subscripts

Symbol	Description	Symbol	Description	Symbol	Description
a	Air	i	Inner hemi-spheroid	r	Radiation
as	Asbestos	o	Outer hemi-spheroid		
eff	Effective	P	Pressure		

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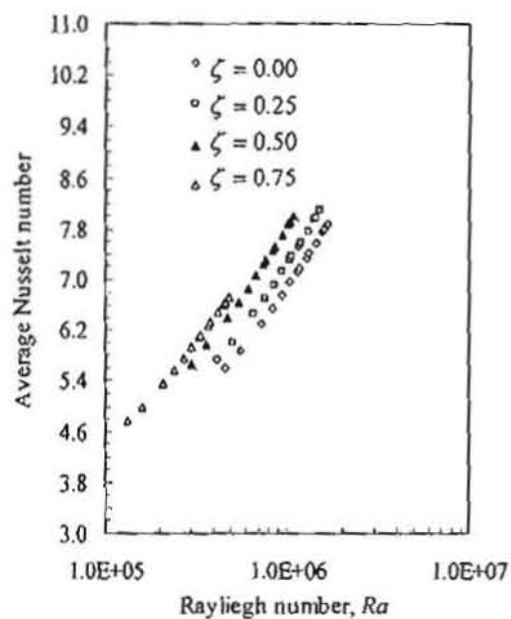


Figure (6), Average Nusselt number versus Rayleigh number for horizontal orientation ($\phi = 0^\circ$, $\varphi = 0^\circ$), for the four tested pairs.

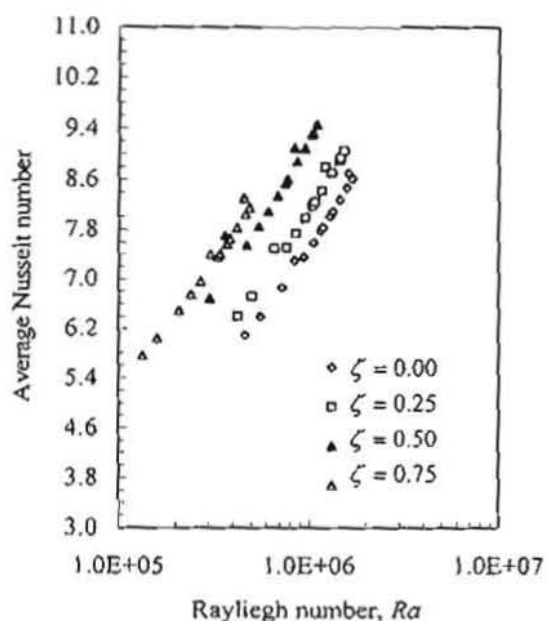


Figure (7), Average Nusselt number versus Rayleigh number for inclined orientation ($\phi = 45^\circ$, $\varphi = 0^\circ$), for the four tested pairs.

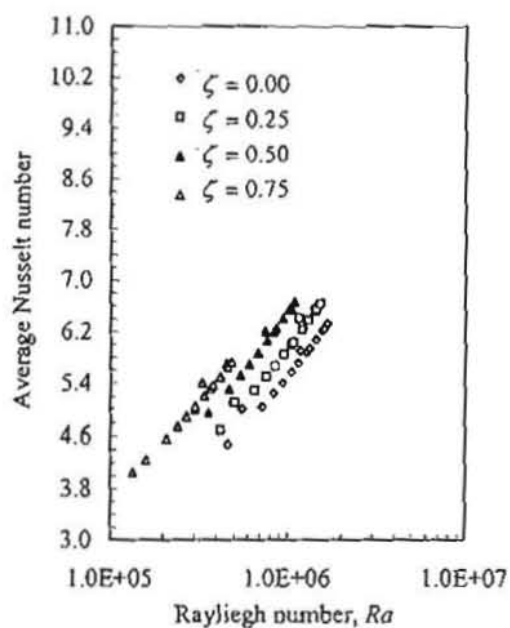


Figure (8), Average Nusselt number versus Rayleigh number for vertical orientation ($\phi = 90^\circ$, $\varphi = 0^\circ$), for the four tested pairs.

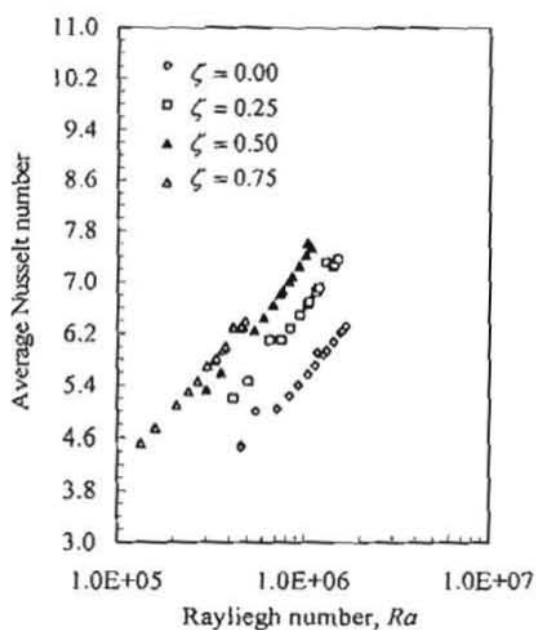


Figure (9), Average Nusselt number versus Rayleigh number for vertical orientation ($\phi = 0^\circ$, $\varphi = 90^\circ$), for the four tested pairs.

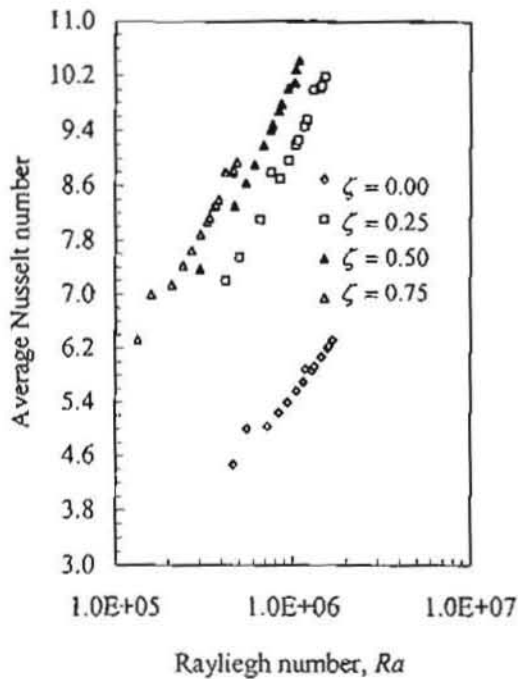


Figure (10), Average Nusselt number versus Rayleigh number for inclined revolved orientation ($\phi = 0^\circ$, $\varphi = 45^\circ$), for the four tested pairs.

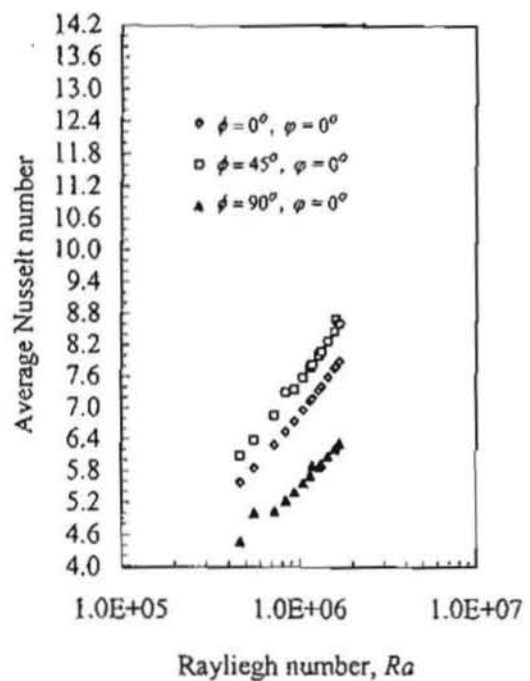


Figure (11), Average Nusselt number versus Rayleigh number for the tested pair No. I for different orientation modes.

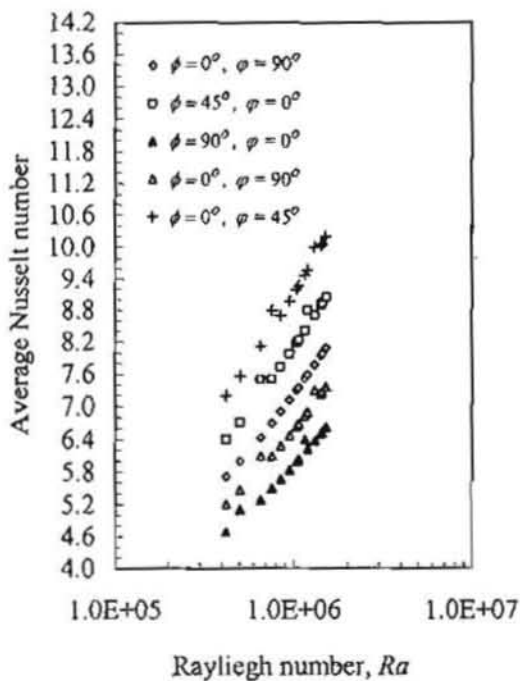


Figure (12), Average Nusselt number versus Rayleigh number for the tested pair No. II for different orientation modes.

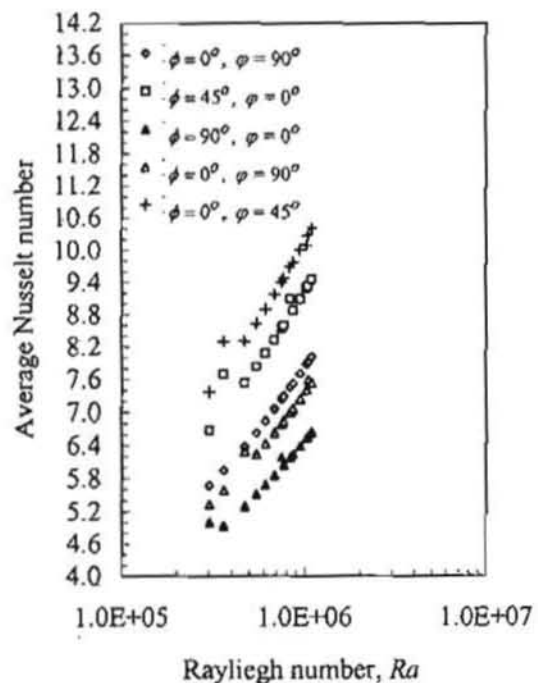


Figure (13), Average Nusselt number versus Rayleigh number for the tested pair No. III for different orientation modes.

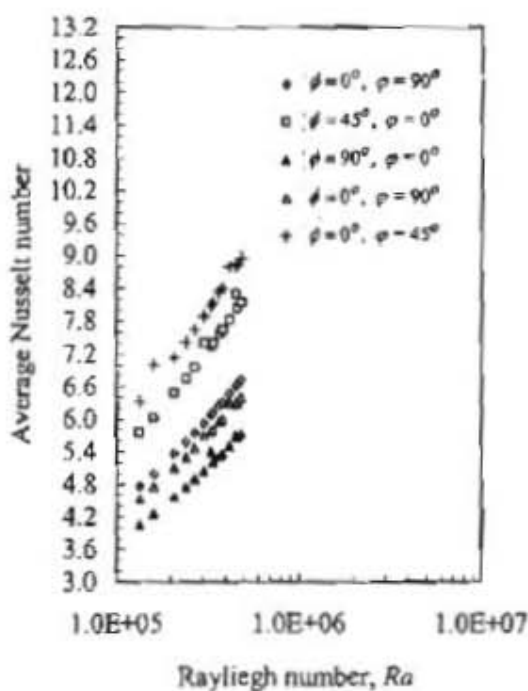


Figure (14), Average Nusselt number versus Rayleigh number for the tested pair No. IV for different orientation modes.

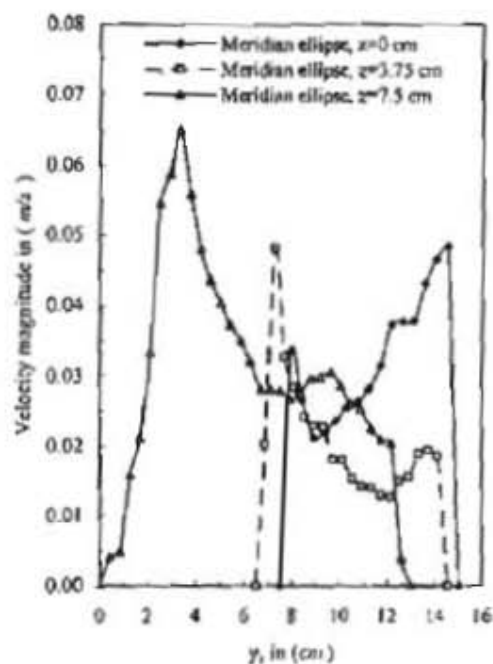


Figure (15), Velocity magnitude versus y -axis in the meridian ellipse at three local z -levels for two concentric hemi-spheres.

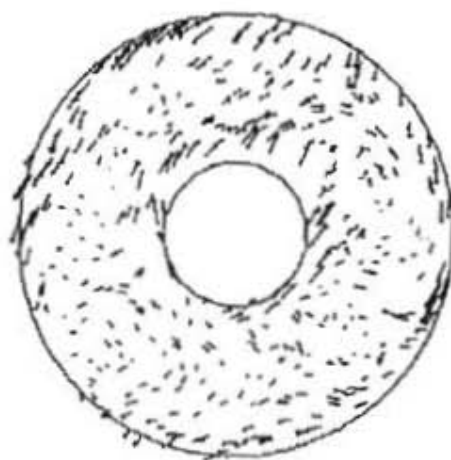


Figure (16), Path lines of air in a y - z plane where $x = -1.5$ cm.

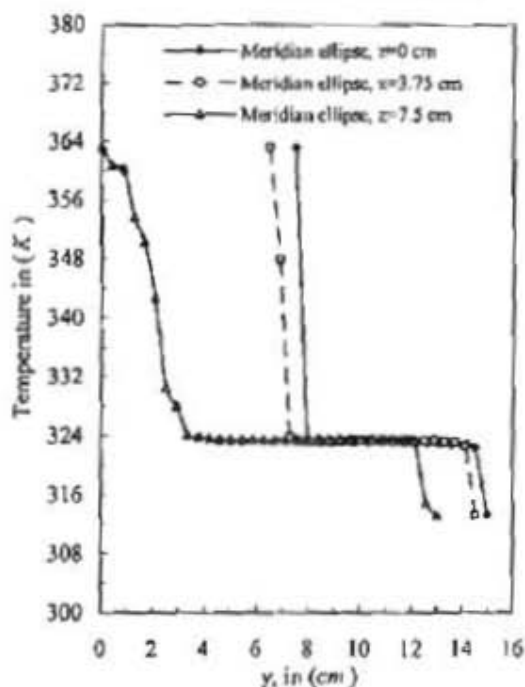


Figure (17), Local temperature versus y -axis at three z values in the meridian ellipse.



Figure (18), Tetrahedral grids on the surface of the two hemi-spheres and the meridian ellipse.

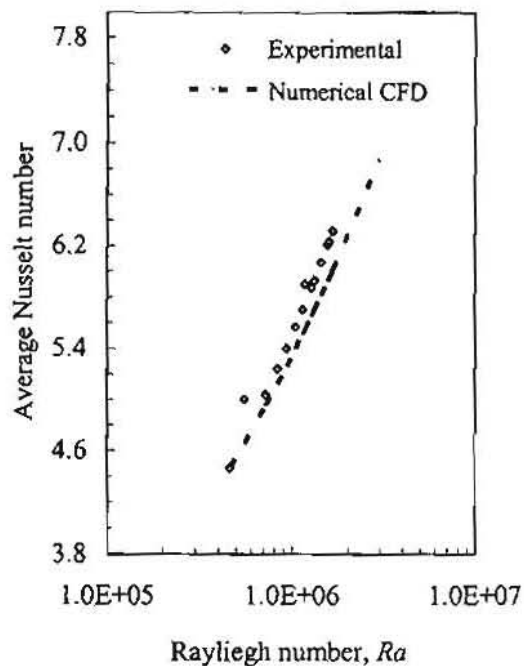


Figure (19), Verification of numerical CFD results with those from experimental tests.

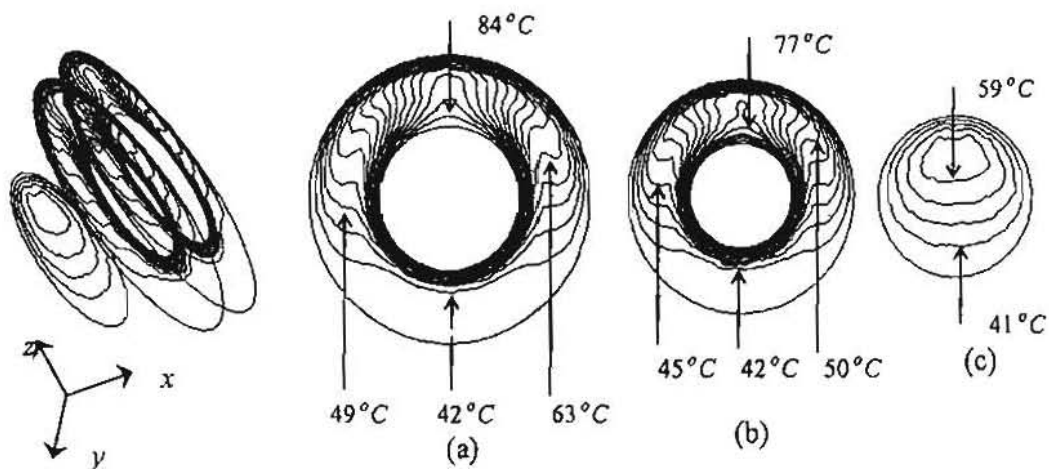


Figure (20), Temperature contours on three successive surfaces along the x -direction, (a) $x=0$, (b) $x = -3.75 \text{ cm}$ and (c) $x = -9 \text{ cm}$.

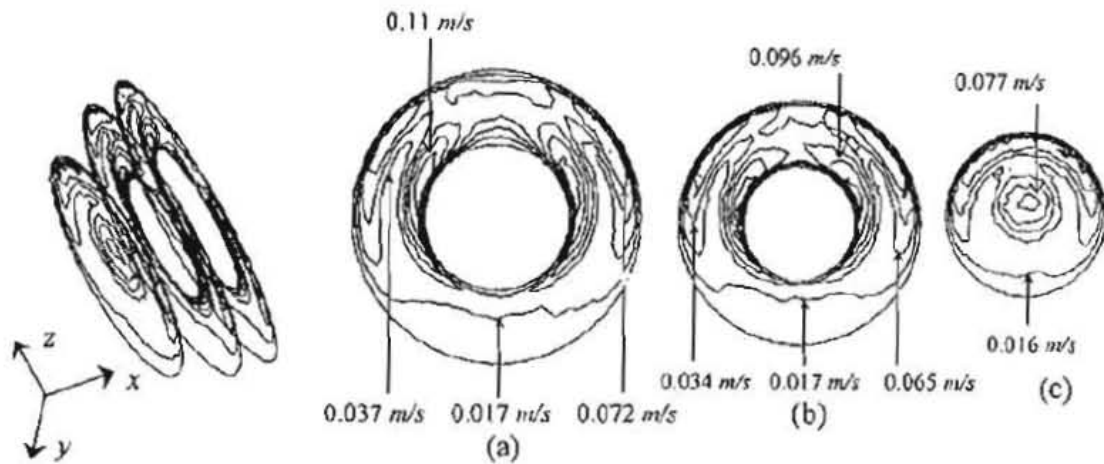


Figure (21), Velocity magnitude contours on three successive surfaces along the x -direction, (a) $x=0$, (b) $x = -3.75$ cm and (c) $x = -9$ cm.

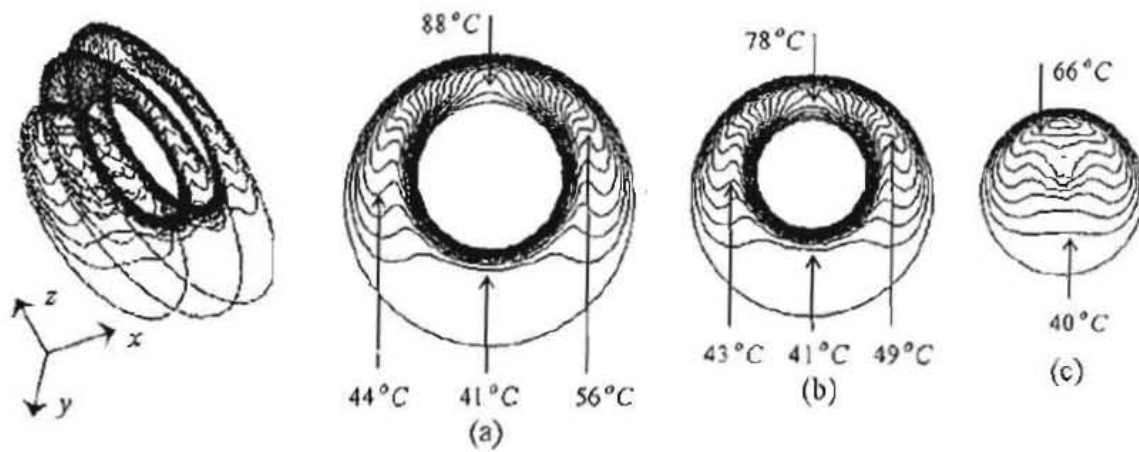


Figure (22), Temperature contours on three successive surfaces along the x -direction for two eccentric spheres with an eccentric distance of 2.5 cm, (a) $x=0$, (b) $x = -3.75$ cm and (c) $x = -9$ cm.

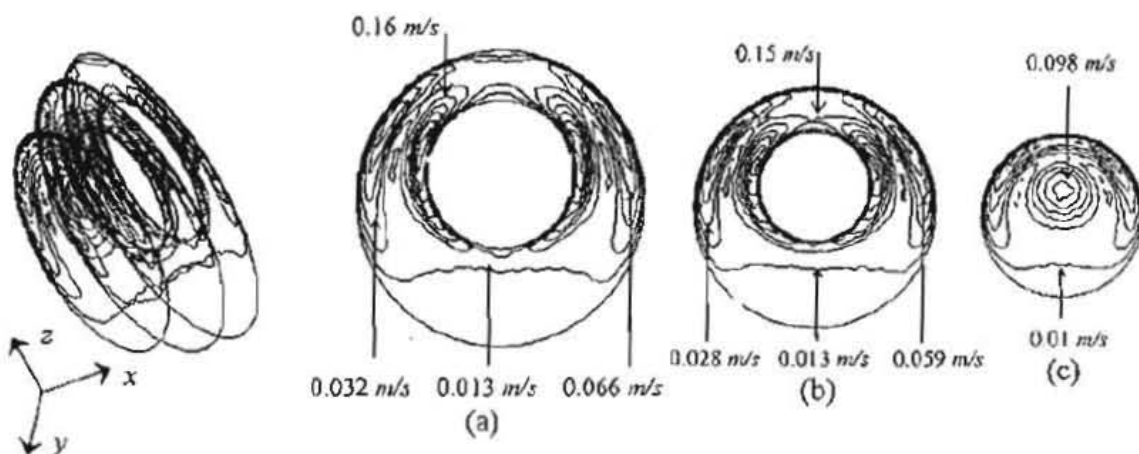


Figure (23), Velocity magnitude contours on three successive surfaces along the x -direction for two eccentric spheres with an eccentric distance of 2.5 cm, (a) $x=0$, (b) $x = -3.75$ cm and (c) $x = -9$ cm.

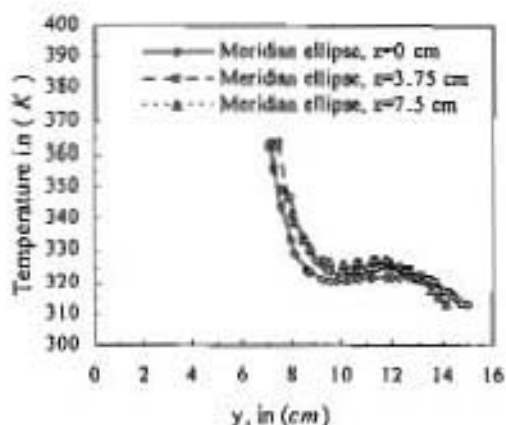


Figure (24), Temperature versus y-axis in the meridian ellipse at three local z-levels for two eccentric hemi-spheres ($e=2.5$ cm).

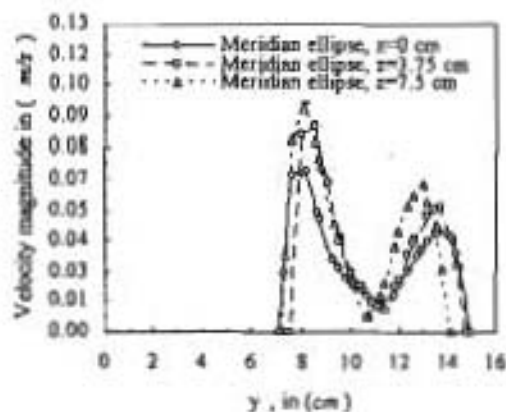


Figure (25), Velocity magnitude versus y in the meridian ellipse at three z-levels for two eccentric hemi-spheres ($e=2.5$ cm).

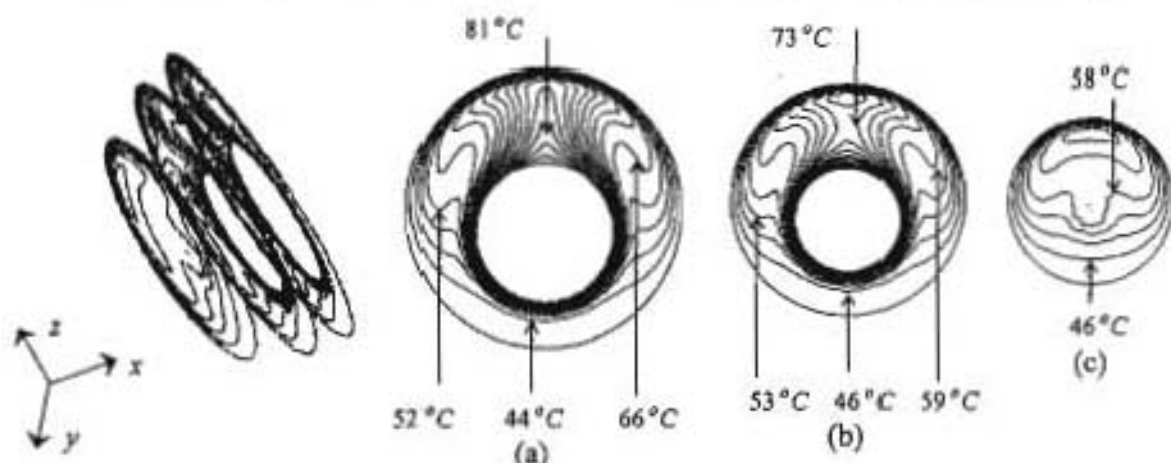


Figure (26), Temperature contours on three successive surfaces along the x-direction for two eccentric spheres with an eccentric distance of (-2.5 cm), (a) $x=0$, (b) $x=-3.75$ cm and (c) $x=-9$ cm.

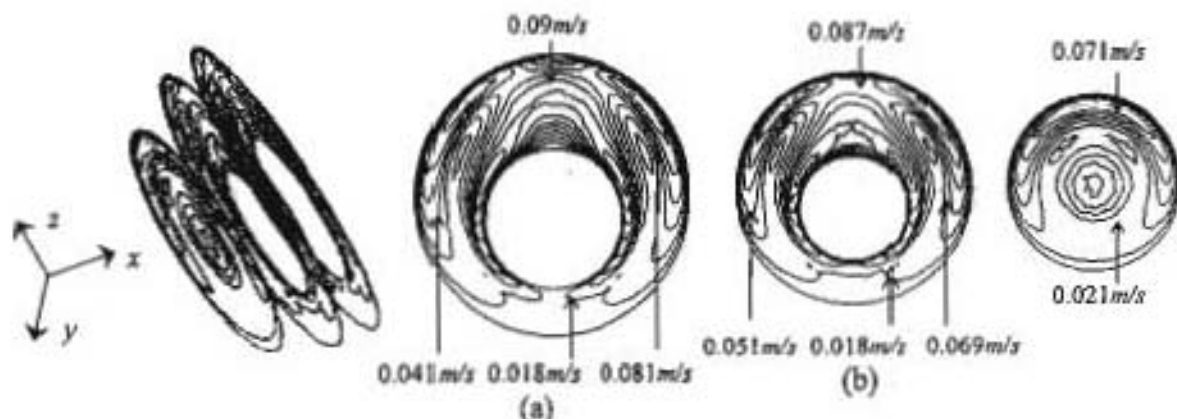


Figure (27), Velocity magnitude contours on three successive surfaces along the x-direction for two eccentric spheres with an eccentric distance of (-2.5 cm), (a) $x=0$, (b) $x=-3.75$ cm and (c) $x=-9$ cm.

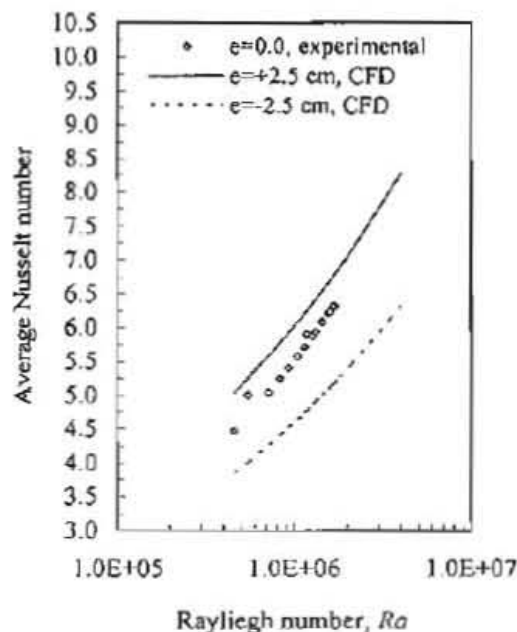


Figure (28), Average Nusselt number versus Rayleigh number for eccentric pair of hemisphere oriented vertically.

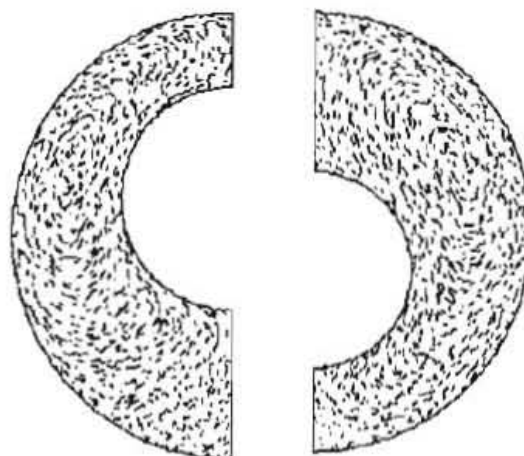


Figure (29), Path lines of air velocity in a two-planes of both positive and negative eccentricities where $x = -2.5$ cm.

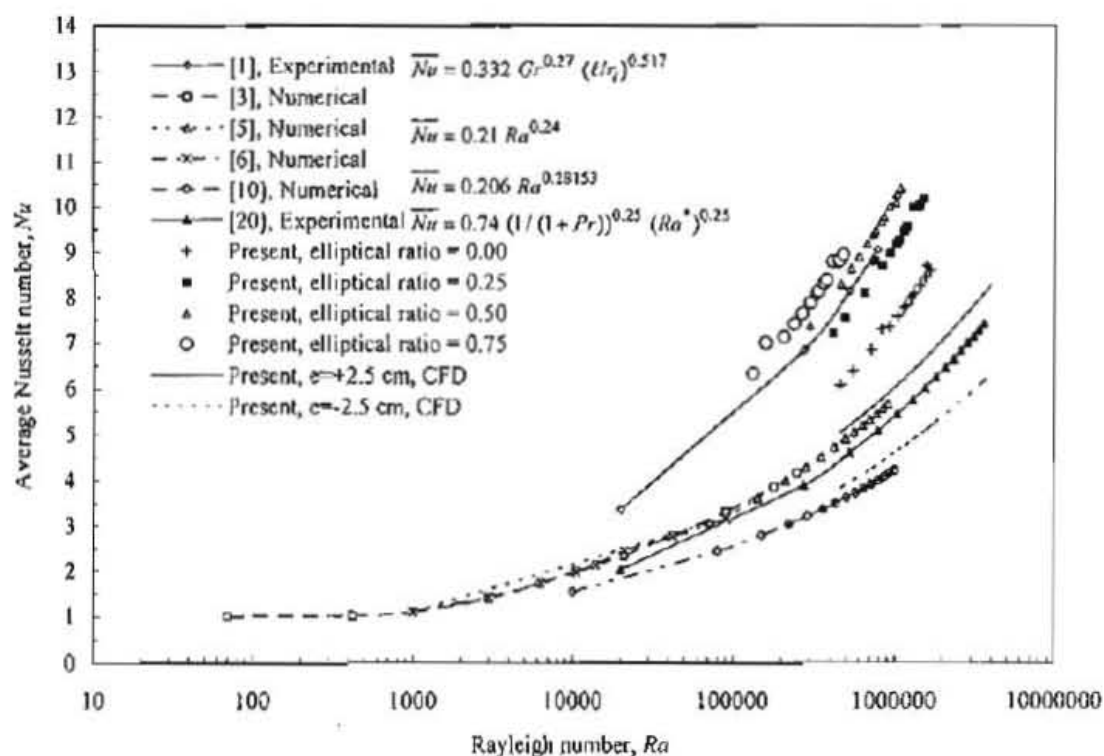


Figure (30), Comparison among results of present attempt and those by the literatures.